## Amendments to the Claims

This listing of claims will replace all prior versions, and listings, of claims in the application:

## **Listing of Claims:**

- 1-10. (Canceled)
- 11. (Original) A method for producing hydrocarbons from synthesis gas in a slurry bubble reactor, the slurry bubble reactor including a liquid and a catalyst at conversion promoting conditions, wherein the liquid has a density,  $\rho_L$ , and viscosity,  $\mu_L$ , under said conversion promoting conditions and wherein the catalyst comprises a plurality of catalyst particles including fresh catalyst particles, the fresh catalyst particles having a particle density,  $\rho_P$ , and particle sizes,  $d_P$ , the method comprising the steps of:
  - (a) selecting the fresh catalyst particles such that the fresh catalyst particles have Archimedes numbers between about 0.02 and about 250, the Archimedes numbers being defined by  $Ar = gd_P^3 \rho_L(\rho_P \rho_L)/\mu_L^2$ ; and
  - (b) passing a synthesis gas feed stream in said slurry bubble reactor over said catalyst under said conversion promoting conditions to convert at least a portion of said synthesis gas feed stream to hydrocarbons.
- 12. (Original) The method of claim 11, wherein a majority of said catalyst particles have particle sizes between about 10 and about 250 microns.
- 13. (Original) The method of claim 12, wherein the catalyst has an effectiveness factor in step (b) greater than about 0.7.
- 14. (Currently amended) The method of claim 12, wherein the catalyst particles have an average Reynolds number of less than about 0.1, according to the equation  $\operatorname{Re}_{avg} = \sum_{i=1}^{M} f_i \operatorname{Re}_i$ ,

where  $\underline{M}$  is the number of different particle size fractions;  $f_i$  is the portion of particles in particle size fraction i, which is determined by dividing the number  $\underline{n}_i$  of particles in size fraction i by the total number  $\underline{N}$  of particles, which is  $\underline{N}$ -determined according to  $\underline{N} = \sum_{i=1}^{M} n_i$  [[,]]; and  $\underline{Re}_i$  is the Reynolds number of particles of size fraction i,  $\underline{Re}_i$  being defined according to the equation  $\underline{Re}_i = \frac{\rho_i v D_i}{\mu_i}$ , where  $\underline{D}_i$  is the number average particle size of particles in size fraction i.

- 15. (Original) The method of claim 11, wherein the fresh catalyst particles have Archimedes numbers between about 0.02 and about 100.
- 16. (Original) The method of claim 11, wherein the fresh catalyst particles have Archimedes numbers between about 0.2 and about 30.
- 17. (Original) The method of claim 11, wherein at least about 90 percent by weight of the catalyst particles have an Archimedes number between about 0.02 and about 100.
- 18. (Currently amended) A process for producing hydrocarbons from synthesis gas in a slurry bubble reactor, the slurry bubble reactor including a liquid and a catalyst at conversion promoting conditions, wherein the liquid has a density,  $\rho_l$ , and viscosity,  $\mu_l$ , under said conversion promoting conditions and wherein the catalyst comprises a plurality of <u>catalyst</u> particles including fresh catalyst particles with a particle velocity,  $\nu$ , the method comprising the steps of:
  - (a) selecting the fresh catalyst particles such that the fresh catalyst particles have Archimedes numbers between about 0.02 and about 250, the Archimedes numbers being defined by  $Ar = gd_P^3 \rho_L(\rho_P \rho_L)/\mu_L^2$ ; and further selecting the catalyst particles such that the catalyst particles have an average Reynolds number of less than about 0.1, according to the equation  $Re_{avg} = \sum_{i=1}^{M} f_i Re_i$ , wherein M is the number of different particle size

fractions:  $f_i$  is the portion of particles in particle size fraction, which is determined by dividing the number  $\underline{n}i$  of particles of size fraction i by the total number N of particles, said N being determined according to

$$N = \sum_{i=1}^{M} n_i [[.]]_i$$
 and  $Re_i$  is the Reynolds number of particles of size fraction

i; Re<sub>i</sub> being defined according to the equation Re<sub>i</sub> =  $\frac{\rho_i v D_i}{\mu_i}$ , where  $D_i$  is

the number average particle size of particles in size fraction i; and

- (b) passing a synthesis gas feed stream in said slurry bubble reactor over said catalyst under said conversion promoting conditions to convert at least a portion of said synthesis gas feed stream to hydrocarbons.
- 19. (Original) The process according to claim 18 wherein the number average particle size is between about 20 and about 50 microns.
- 20. (Original) The process according to claim 19 wherein the number average particle size is between about 30 and about 40 microns.
- 21. (Original) The process according to claim 19, wherein the catalyst has an effectiveness factor in step (b) greater than about 0.7.
- 22. (Original) The process according to claim 18 wherein at least 90% of the plurality of particles have sizes between about 20 and about 150 microns.
- 23. (Original) The process according to claim 18 wherein the plurality of particles comprise a substantially log normal distribution of volume percent of catalyst particles versus particle sizes.
- 24. (Original) The process according to claim 18 wherein the plurality of particles have an average Reynolds number of between about 0.05 and about 0.06.

- 25. (New) The process according to claim 11 wherein the catalyst comprises a number average particle size between about 20 and about 50 microns.
- 26. (New) The process according to claim 11 wherein the catalyst comprises a number average particle size between about 30 and about 40 microns.
- 27. (New) The process according to claim 11 wherein at least 90% of the plurality of particles have sizes between about 20 and about 150 microns.
- 28. (New) The process according to claim 14 wherein the plurality of particles have an average Reynolds number of between about 0.05 and about 0.06.
- 29. (New) A method for producing hydrocarbons from synthesis gas in a slurry bubble reactor, the slurry bubble reactor including a liquid and a catalyst at conversion promoting conditions, wherein the liquid has a density,  $\rho_L$ , and viscosity,  $\mu_L$ , under said conversion promoting conditions and wherein the catalyst comprises a plurality of catalyst particles including fresh catalyst particles, the fresh catalyst particles having a particle density,  $\rho_P$ , and particle sizes,  $d_P$ , the method comprising the steps of:
  - (a) selecting the fresh catalyst particles such that the fresh catalyst particles have Archimedes numbers between about 0.02 and about 250, the Archimedes numbers being defined by  $Ar = gd_P^3 \rho_L(\rho_P \rho_L)/\mu_L^2$ ; and
  - (b) passing a synthesis gas feed stream in said slurry bubble reactor over said catalyst under said conversion promoting conditions to convert at least a portion of said synthesis gas feed stream to hydrocarbons, while maintaining a catalyst nonuniformity in said reactor of less than 4.
- 30. (New) The process of claim 29, wherein the catalyst non-uniformity is less than about 3.
- 31. (New) The process of claim 29, wherein the catalyst non-uniformity is less than about 2.

- 32. (New) The process of claim 29, wherein the fresh catalyst particles have Archimedes numbers between about 0.02 and about 100.
- 33. (New) The process of claim 29, wherein the fresh catalyst particles have Archimedes numbers between about 0.2 and about 30.
- 34. (New) The process of claim 29, wherein at least about 90 percent by weight of the catalyst particles in said reactor have an Archimedes number between about 0.02 and about 100.